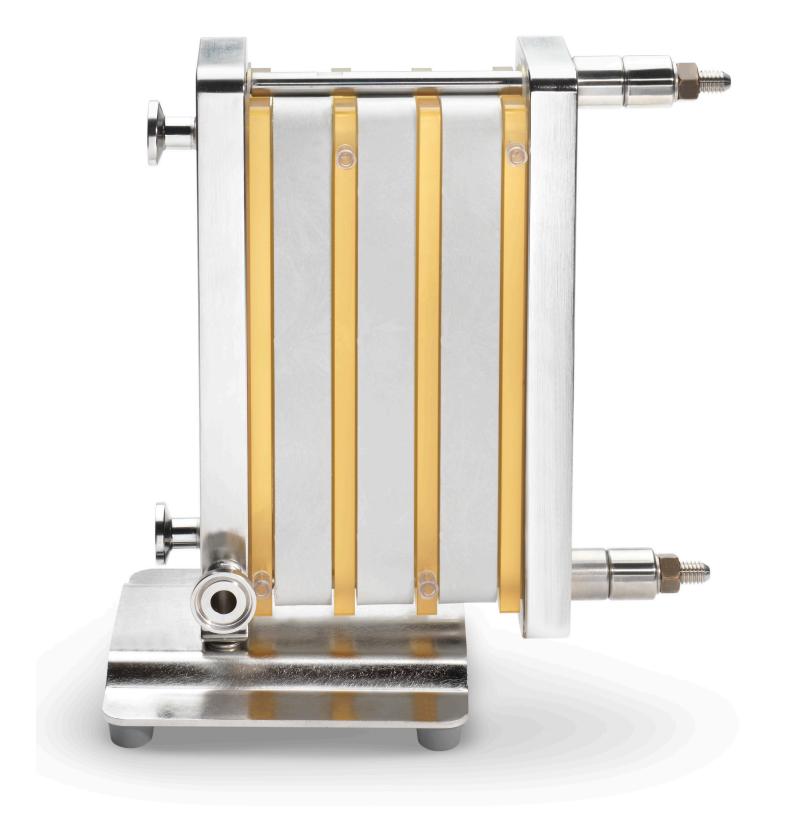
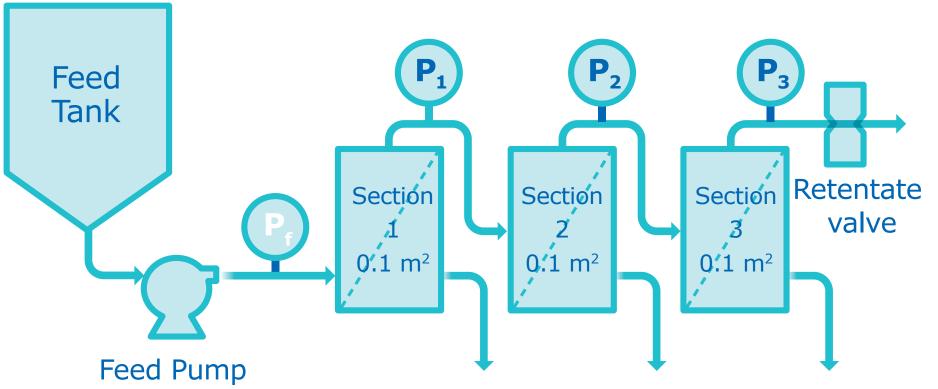
Single Pass Tangential Flow Filtration (SPTFF)



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Scale down SPTFF testing

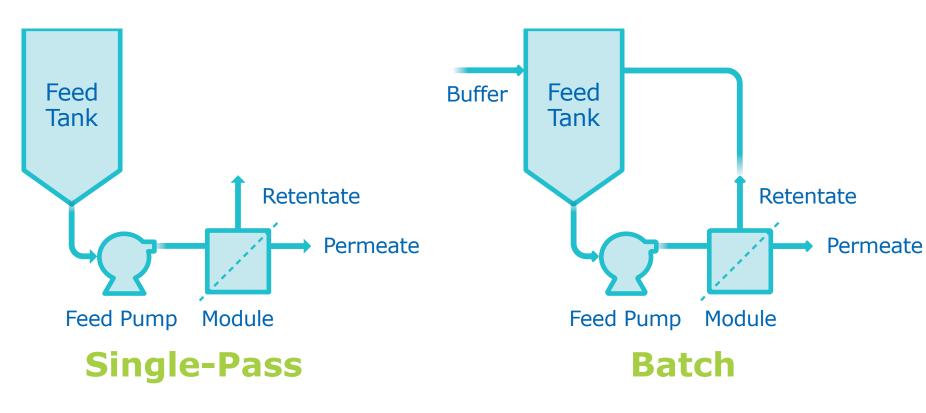


How does SPTFF compare with current batch UF?

- Both use same cassettes and holders (need diverter plates)
- Simplicity comes at a price: e.g. 1.2 3X membrane area versus batch sizing

Application	SPTFF
Intermediate UF, 19 g/L to 40 g/L	0.82 LMM*

What is SPTFF?



- Product is sufficiently concentrated/diafiltered after a single pass through filter assembly
- No retentate return needed
- Continuous operation
- Product is *not* sufficiently concentrated/diafiltered after a single pass
- Requires retentate return and multiple passes through filter
- Batch operation

How does SPTFF work?

• **Batch processing:** High feed flux and TFF devices operated in parallel results in low fluid residence time in membrane channels, hence low conversion

Separate permeate lines for each section

• Recovery flush

• Feed flow excursions

• Cleaning & NWP recovery

- Three Pellicon[®] 3 PLCTK 0.1m² cassettes
- Diverter plates
- Recycled retentate/permeates



Final Formulation UF1, 18 g/L to 73 g/L	0.36 LMM
Final Formulation UF2, 77 g/L to 174 g/L	0.18 LMM

*LMM = feed flow rate in liters per minute per total square meters of membrane area.

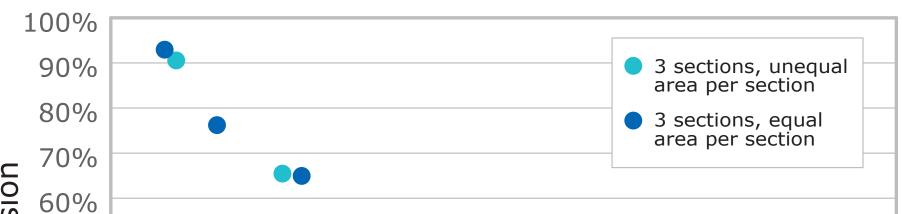
This is worth it for:

- Plants where product pool volumes have increased beyond available tank capacities
- Limited plant footprint (no room for batch operation)
- Batch holdup limits final concentration (can't get to target product g/L)

Is there an advantage to using custom SPTFF modules or systems?

• Sizing is comparable between equal area sections & in sections in series

• Equal area sectioning is well known and in the public domain



- 1 device in series
- feed flux ~ 6 LMM
- conversion ~ 15 20%
- **SP-TFF processing:** Increase conversion by increasing fluid residence time in membrane channels via lower feed flux and longer channels
 - 1 to 3 (or more) devices in series
 - feed flux ~ 0.5 LMM or less
 - conversion $\sim 75 90 + \%$

Why use SPTFF?

• Simple operation

- Constant feed flow & retentate pressure
- Leverage existing holders
- Simple system design
 - Smaller pump
 - Smaller footprint
 - Low working volume allows higher final concentrations
 - Simplifies product recovery

Once-through flowpath

- Run in-line with other unit operations
- Enables continuous processing
- Reduces pumping damage for sensitive products

Where can SPTFF be used?



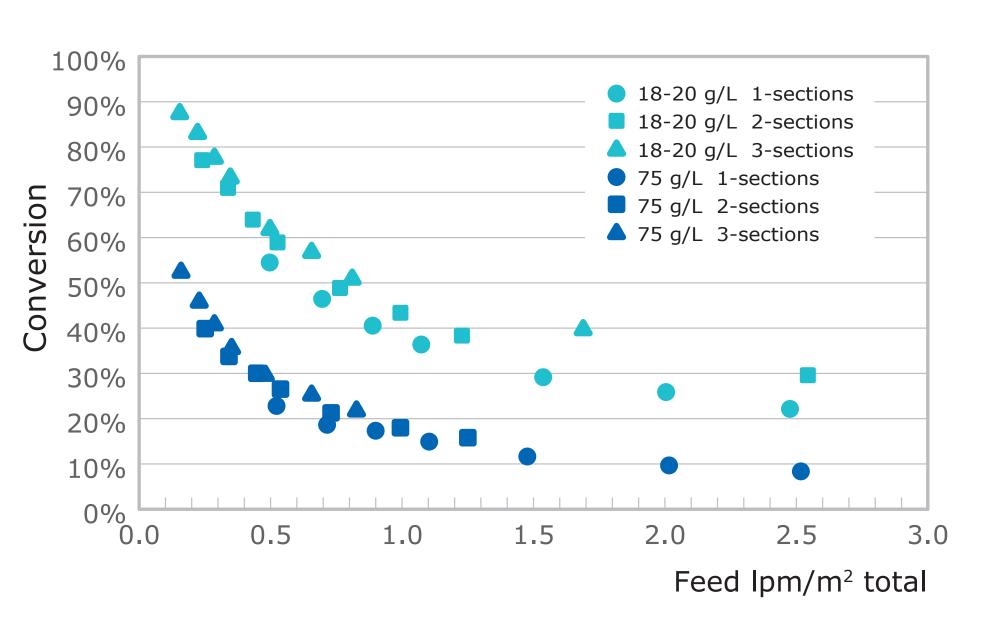
Retentate

Filtrate

SPTFF sizing with IVIG

• Conversion

- Decreases with increasing feed LMH
- Increases with *#* in series
- Decreases with feed g/L



• Sizing

- feed flux based on

process time

conversion target

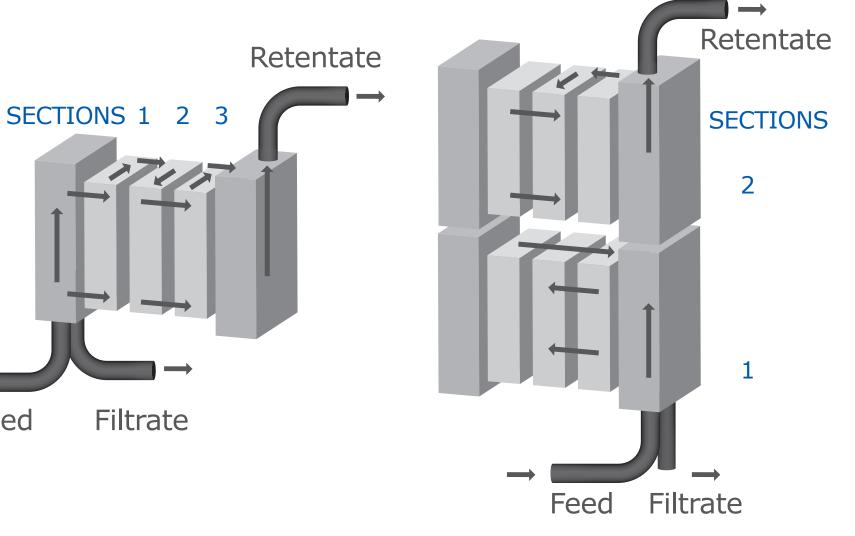
- membrane area based

on batch volume and

Conversion 50% 40% 30% 20% 10% 0% 0.5 2.5 3.0 1.0 1.5 2.0 Feed lpm/m² total

Scaling Options

- Existing holders and cassettes
- Operation at lower flows



SPTFF cleaning after IVIG

• Repeatable NWP recovery for all 3 cassettes in series after use

Single level

Feed

Multiple level

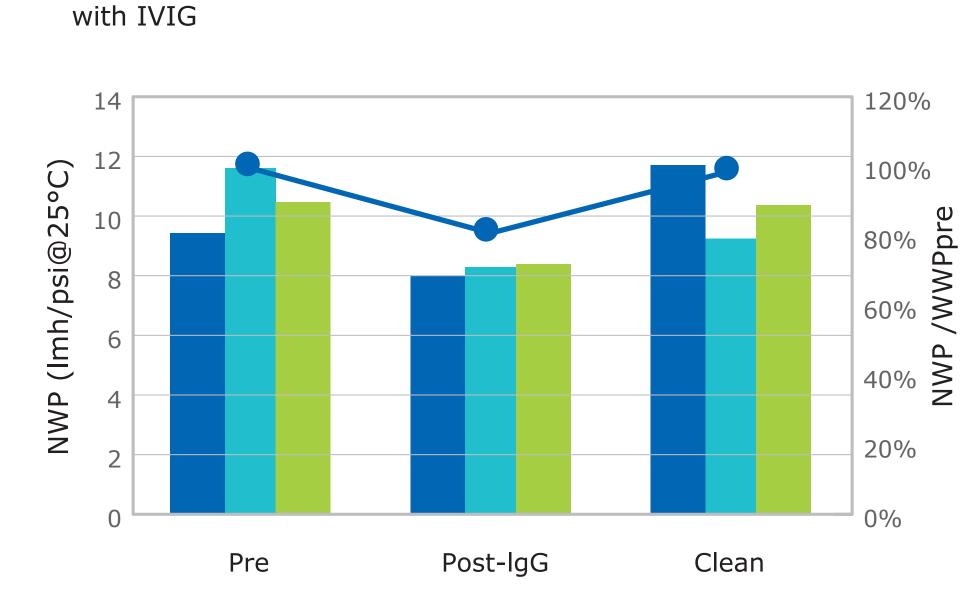
Feed Filtrate Diafiltrate Retentate Feed

Filtrate

• Reduce or eliminate intermediate pool tank

Pre-column (or other step) concentration/ diafiltration

- Desalt before IEX column or virus prefilter
- Concentrate to increase capacity and reduce time
- **Final formulation UF2 step** (post batch UF/DF)
- Avoid working volume limits Maintain product quality, particularly if the product is heated to overcome viscosity effects





Horizontal sectioning

• Separator plates

Vertical sectioning

Acknowledgments

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